

Supplementary information

Addressing the role of methodological inconsistencies in bio-based plastic LCAs: a case study for bio-based PE and bio-based PET

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| Indicator | Description | Page |
|------------|---|-------|
| Figure S.1 | System diagram for bio-PE and bio-PET, marking the three variables considered in this study and indicating the LCI table with the corresponding scenario. | 2 |
| Table S.1 | Lifecycle inventory for SC-BR-1. | 2 |
| Table S.2 | Lifecycle inventory for SC-BR-2. | 3 |
| Table S.3 | Lifecycle inventory for SC-BR-3. | 3 |
| Table S.4 | Lifecycle inventory for SC-BR-4. | 4 |
| Table S.5 | Lifecycle inventory for SCM-IN. | 4-5 |
| Table S.6 | Lifecycle inventory for SB-BE. | 5 |
| Table S.7 | Lifecycle inventory for SB-RER. | 6 |
| Table S.8 | Lifecycle inventory for WH-BE. | 6 |
| Table S.9 | Lifecycle inventory for WH-RER. | 6 |
| Table S.10 | Lifecycle inventory for M-RER. | 7 |
| Table S.11 | Lifecycle inventory for M-US. | 7 |
| Table S.12 | Lifecycle inventory for ethylene 1 (base). | 7 |
| Table S.13 | Lifecycle inventory for ethylene 2. | 7 |
| Table S.14 | Lifecycle inventory for ethylene 3. | 8 |
| Table S.15 | Lifecycle inventory for ethylene 4. | 8 |
| Table S.16 | Lifecycle inventory for TA-petro (base). | 8 |
| Table S.17 | Lifecycle inventory for TA-WH. | 8 |
| Table S.18 | Lifecycle inventory for TA-M. | 9 |
| Table S.19 | Lifecycle inventory for TA-WO | 9-10 |
| Table S.20 | Lifecycle inventory for bio-MEG production. | 10 |
| Table S.21 | Lifecycle inventory for bio-HDPE production. | 10 |
| Table S.22 | Lifecycle inventory for bio-PET production. | 10 |
| Figure S.2 | Environmental impact of bio-based and petrochemical-based HDPE and PET when changing the biomass cultivation and ethanol production. | 11-16 |
| Figure S.3 | Environmental impact of bio-based and petrochemical-based HDPE and PET when changing the ethylene production. | 17-22 |
| Figure S.4 | Environmental impact of bio-based and petrochemical-based PET when changing TA production. | 23-25 |

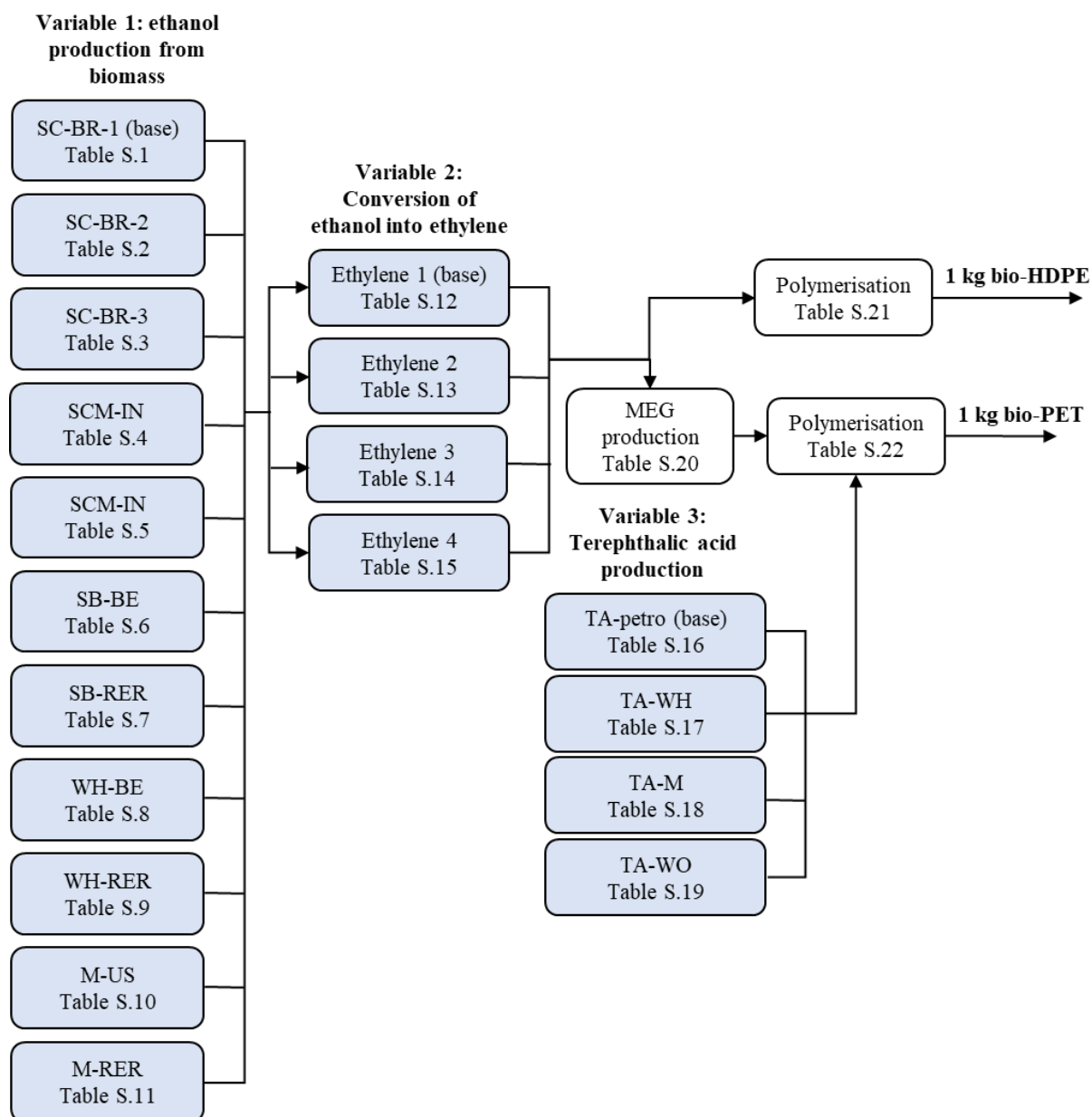


Figure S.1: System diagram for bio-PE and bio-PET, marking the three variables considered in this study and indicating the LCI table with the corresponding scenario.

Table S.1: Lifecycle inventory for SC-BR-1 (base).

| Biomass cultivation – 1 kg | | |
|----------------------------|--|-------------|
| Amount | Activity | Adjustments |
| 1 kg | Market for sugarcane [BR] | None |
| Ethanol production – 1 kg | | |
| Amount | Activity | Adjustments |
| 1 kg | Ethanol, without water, in 99.7% solution state, from fermentation | None |

Table S.2: Lifecycle inventory for SC-BR-2.

| Biomass cultivation: Sugarcane [BR] – 1000 kg | | |
|--|---|--------------------|
| Amount | Activity | Adjustments |
| 147 m ² a | Agricultural land occupation, permanent crop, non-irrigated | |
| 0.11 kg | ammonia, anhydrous, liquid [BR] | |
| 0.29 kg | ammonium nitrate [GLO] | |
| 0.37 kg | Urea [BR] | |
| 0.08 kg | monoammonium phosphate [BR] | |
| 0.146 kg | single superphosphate [RoW] | |
| 0.081 kg | triple superphosphate [BR] | |
| 0.003 kg | phosphate rock, beneficiated [GLO] | |
| 0.022 kg | monoammonium phosphate [BR] | |
| 0.96 kg | potassium chloride [RoW] | |
| 0.01 kg | potassium nitrate [RoW] | |
| 0.01 kg | potassium sulfate [BR] | |
| 0.03901 kg | pesticide, unspecified [RoW] | |
| 0.006 kg | triazine-compound, unspecified [BR] | |
| 0.001 kg | phenoxy-compound [GLO] | |
| 0.002 kg | Glyphosate [RoW] | |
| 5.18 kg | Lime [GLO] | |
| 2.0 kg | hard coal ash [GLO] | |
| 2.3 kg | gypsum, mineral [BR] | |
| 31.0 kg | filter cake, from sugarcane juice filtration [GLO] | |
| 3.6256 kg | Diesel [BR] | |
| Ethanol production – 1 kg | | |
| Amount | Activity | Adjustments |
| 14 985 kg | Sugarcane [BR] | |
| 0.15 kg | lubricating oil [RoW] | |
| 13.1 kg | Lime [RoW] | |
| 9.3 kg | sulfuric acid [RoW] | |
| 0.1 kg | pesticide, unspecified [RoW] | |
| 0.86 kg | chemical, organic [GLO] | |
| 24.7 kg | tap water [BR] | |
| 8.32 t km | transport, tractor and trailer, agricultural [RoW] | |
| -130.0 kg | bagasse, from sugarcane [BR] | |
| -60.0 kWh | electricity, medium voltage [BR] | |

Table S.3: Lifecycle inventory for SC-BR-3.

| Biomass cultivation – 1 kg | | |
|-----------------------------------|--|--------------------|
| Amount | Activity | Adjustments |
| 1 kg | Market for sugarcane [BR] | None |
| Ethanol production – 1 kg | | |
| Amount | Activity | Adjustments |
| 1 kg | Ethanol, without water, in 99.7% solution state, from fermentation | None |

Table S.4: Lifecycle inventory for SC-BR-4.

| Biomass cultivation: sugarcane [BR] – 25.5 kg | | |
|--|---|--------------------|
| Amount | Activity | Adjustments |
| 5.2 MJ | diesel, burned in agricultural machinery [GLO] | |
| 0.0103 kg | chemical, inorganic [GLO] | |
| 147 m ² a | Agricultural land occupation, permanent crop, non-irrigated | |
| Ethanol production – 1.7 kg | | |
| Amount | Activity | Adjustments |
| 12.11 kg | Sugarcane [BR] | |
| 49.5 MJ | Heat, district or industrial, from bagasse [BR] | |

Table S.5: Lifecycle inventory for SCM-IN.

| Sugarcane production – 1000 kg* | | |
|--|---|--------------------|
| Amount | Activity | Adjustments |
| 169 m ² a | Land occupation, permanent crop, irrigated | |
| 59.5 m ³ | Irrigation [IN] | |
| 0.42 kg | ammonium sulfate [RoW] | |
| 0.42 kg | ammonium nitrate [RoW] | |
| 0.37 kg | diammonium phosphate [RoW] | |
| 1.23 kg | urea [RoW] | |
| 0.25 kg | potassium nitrate [RoW] | |
| 0.62 kg | diammonium phosphate [RoW] | |
| 0.4 kg | single superphosphate [RoW] | |
| 0.2 kg | triple superphosphate [RoW] | |
| 0.07 kg | phosphate rock, beneficiated [RoW] | |
| 0.8 kg | potassium chloride [RoW] | |
| 0.008 kg | potassium nitrate [RoW] | |
| 0.008 kg | potassium sulfate [RoW] | |
| 0.118 kg | pesticide, unspecified [RoW] | |
| 0.011 kg | triazine-compound, unspecified [RoW] | |
| 0.003 kg | phenoxy-compound [RoW] | |
| 0.004 kg | glyphosate [RoW] | |
| 2.0 kg | hard coal ash [RoW] | |
| 40.0 kg | filter cake, from sugarcane juice filtration [GLO] | |
| 0.5441 kg | Diesel [IN] | |
| 12.0 kWh | electricity, medium voltage [IN] | |
| Processing into sugarcane molasses – 50.3 kg* | | |
| Amount | Activity | Adjustments |
| 1000.0 kg | Sugarcane production, from SC-BR-2 [IN] | |
| 1.5 kg | sulfur dioxide, liquid [RoW] | |
| 1.9 kg | limestone, unprocessed [RoW] | |
| 0.5 kg | sodium hydroxide, without water, in 50% solution state [GLO] | |
| 0.1 kg | single superphosphate [RoW] | |
| 0.03 kg | soda ash, dense [GLO] | |
| 0.01 kg | chemical, organic [GLO] | |
| 0.6 kg | lubricating oil [RoW] | |
| 0.01 kg | phosphoric acid, fertiliser grade, without water, in 70% solution state [RoW] | |
| 30.0 kg | tap water [IN] | |
| 12.6 t km | transport, freight train [IN] | |

| | | |
|-------------------------------------|---|--------------------|
| -54.2 kWh | electricity, medium voltage [IN] | |
| Ethanol production – 1000 kg | | |
| Amount | Activity | Adjustments |
| 446.08 kg | Sugarcane molasses [IN] | |
| 0.41 kg | sulfuric acid [RoW] | |
| 0.11 kg | magnesium sulfate [RoW] | |
| 1.3 kg | urea [RoW] | |
| 0.14 kg | phosphoric acid, industrial grade, without water, in 85% solution state [RoW] | |
| 0.38 kg | chlorine, liquid [RoW] | |
| 0.06 kg | sodium bicarbonate [RoW] | |
| 0.1 kg | chromium oxide, flakes [RoW] | |
| 0.6 kg | sodium hydroxide, without water, in 50% solution state [GLO] | |
| 0.12 kg | Zinc [GLO] | |
| 0.02 kg | Formaldehyde [RoW] | |
| 11.4 kg | tap water [IN] | |
| 380.0 t km | transport, freight train [IN] | |

* Economic allocation was used for the processing of sugarcane, resulting in 8.8% being allocated to sugarcane molasses.

Table S.6: Lifecycle inventory for SB-BE.

| | | |
|---------------------------------------|--|--------------------|
| Biomass cultivation – 1000 kg* | | |
| Amount | Activity | Adjustments |
| 1.52 kg | inorganic nitrogen fertiliser, as N [BE] | |
| 2.53 kg | inorganic potassium fertiliser, as K ₂ O [BE] | |
| 1.10 kg | inorganic phosphorus fertiliser, as P ₂ O ₅ [BE] | |
| 0.04 kg | pesticide, unspecified [RER] | |
| 2.05 kg | Diesel [Europe without Switzerland] | |
| 13.69 m ² a | Land occupation, permanent crop, non-irrigated | |
| Ethanol production – 783 kg* | | |
| Amount | Activity | Adjustments |
| 9904 kg | Sugar beet [BE] | |
| 163.0 kWh | electricity, medium voltage [BE] | |
| 6248.0 MJ | heat, district or industrial, natural gas [BE] | |
| 0.3 kg | lubricating oil [RER] | |
| 191.5 kg | lime [RER] | |
| 7.4 kg | sulfuric acid [RER] | |
| 0.25 kg | hydrochloric acid, without water, in 30% solution state [RER] | |
| 10.6 kg | gypsum, mineral [RER] | |
| 0.55 kg | EDTA, ethylenediaminetetraacetic acid [RER] | |
| 0.5 kg | sodium bicarbonate [RER] | |

*Using economic allocation, 84% of impacts are allocated to ethanol from sugar beet.

Table S.7: Lifecycle inventory for SB-RER.

| Biomass cultivation – 100 kg | | |
|------------------------------|--|-------------|
| Amount | Activity | Adjustments |
| 59 kg | Sugar beet production [FR] | |
| 41 kg | Sugar beet production [DE] | |
| Ethanol production – 1 kg | | |
| Amount | Activity | Adjustments |
| 11.22 | Sugar beet [RER] | |
| 1.03 MJ | heat, from steam, in chemical industry [RER] | |
| 0.00505 kg | ammonia, anhydrous, liquid [RER] | |
| 0.0101 kg | sodium hydroxide, without water, in 50% solution state [GLO] | |
| 0.0193 kg | sulfuric acid [RER] | |

Table S.8: Lifecycle inventory for WH-BE.

| Biomass cultivation – 1000 kg* | | |
|--------------------------------|--|-------------|
| Amount | Activity | Adjustments |
| 19.65 kg | inorganic nitrogen fertiliser, as N [BE] | |
| 10.81 kg | inorganic potassium fertiliser, as K ₂ O [BE] | |
| 6.63 kg | inorganic phosphorus fertiliser, as P ₂ O ₅ [BE] | |
| 0.36 kg | pesticide, unspecified [RER] | |
| 9.19 kg | Diesel [Europe without Switzerland] | |
| 116.28 m ² a | Land occupation | |
| Ethanol production – 783 kg | | |
| Amount | Activity | Adjustments |
| 2905 kg | Wheat [BE] | |
| 235.0 kWh | electricity, medium voltage [BE] | |
| 1800.0 MJ | heat, district or industrial, natural gas [BE] | |
| 1.7 kg | sulfuric acid [RER] | |
| 6.65 kg | sodium bicarbonate [RER] | |
| 0.21 kg | magnesium sulfate [RER] | |
| 3.6 kg | ammonia, anhydrous, liquid [RER] | |

*Using economic allocation, 67% of impacts are allocated to ethanol from wheat.

Table S.9: Lifecycle inventory for WH-RER.

| Biomass cultivation – 100 kg | | |
|------------------------------|--|-------------|
| Amount | Activity | Adjustments |
| 41.7 kg | Wheat grain [FR] | |
| 58.3 kg | Wheat grain [DE] | |
| Ethanol production – 1 kg | | |
| Amount | Activity | Adjustments |
| 3.73 kg | Wheat [RER] | |
| 13.6 MJ | heat, from steam, in chemical industry [RER] | |
| 0.64 kWh | electricity, medium voltage [RER] | |
| 0.0101 kg | sodium hydroxide, without water, in 50% solution state [GLO] | |
| 0.00505 kg | ammonia, anhydrous, liquid [RER] | |
| 0.0193 kg | sulfuric acid [RER] | |

Table S.10: Lifecycle inventory for M-RER.

| Biomass cultivation – 1 kg | | |
|----------------------------|--|-------------|
| Amount | Activity | Adjustments |
| 1 kg | Maize grain, feed, Swiss integrated production [CH] | |
| Ethanol production – 1 kg | | |
| Amount | Activity | Adjustments |
| 2.55 kg | Maize [RER] | |
| 11.85 MJ | heat, from steam, in chemical industry [RER] | |
| 0.27 kWh | electricity, medium voltage [RER] | |
| 0.0061 kg | ammonia, anhydrous, liquid [RER] | |
| 0.0101 kg | sodium hydroxide, without water, in 50% solution state [GLO] | |
| 0.0027 kg | quicklime, milled, packed [RER] | |
| 0.0033 kg | sulfuric acid [RER] | |
| 0.0011 kg | urea [RER] | |

Table S.11: Lifecycle inventory for M-US.

| Biomass cultivation – 1 kg | | |
|----------------------------|---|-------------|
| Amount | Activity | Adjustments |
| 1 kg | Maize grain production [US] | |
| Ethanol production – 1 kg | | |
| Amount | Activity | Adjustments |
| 1 kg | ethanol, without water, in 99.7% solution state, from fermentation [US] | |

Table S.12: Lifecycle inventory for ethylene 1 (base).

| Ethylene production – 1kg | | |
|---------------------------|---|-------------|
| Amount | Activity | Adjustments |
| 2.08 kg | Ethanol | |
| 0.1044 kg | nitrogen, liquid [RoW] | |
| 0.11 kg | zeolite, powder [RoW] | |
| 0.0266 kg | sodium bicarbonate [RoW] | |
| 2.57 kg | tap water [BR] | |
| 0.0035 kg | Propylene [RoW] | |
| 0.47 kWh | electricity, medium voltage [BR] | |
| 4.84 MJ | heat, district or industrial, from Bagasse [BR] | |

Table S.13: Lifecycle inventory for ethylene 2.

| Ethylene production – 783 kg | | |
|------------------------------|--|-------------|
| Amount | Activity | Adjustments |
| 1.06 kg | Ethanol | |
| 1210 kg | steam, in chemical industry [RER] | |
| 340 kWh | electricity, medium voltage [BE] | |
| 200 MJ | heat, district or industrial, natural gas [BE] | |

Table S.14: Lifecycle inventory for ethylene 3.

| Ethylene production – 1kg | | |
|---------------------------|--|-------------|
| Amount | Activity | Adjustments |
| 1.70 kg | Ethanol | |
| 5.6 MJ | heat, district or industrial, other than natural gas, Bagasse [BR] | |
| 0.5 kWh | electricity, medium voltage [BR] | |

Table S.15: Lifecycle inventory for ethylene 4.

| Ethylene production – 1kg | | |
|---------------------------|---|--|
| Amount | Activity | Adjustments |
| 1.65 kg | Ethanol | |
| 0.32 kWh | electricity, medium voltage [US] | |
| Polymerisation – 1kg | | |
| Amount | Activity | Adjustments |
| 1 kg | Polyethylene, high density, granulate [RoW] | Replacing petrochemical ethylene with bio-based ethylene, using the Brazilian market for electricity |

Table S.17: Lifecycle inventory for TA-petro (base).

| Terephthalic acid production – 1 kg | | |
|-------------------------------------|----------------------------|---------------------------------------|
| 1 kg | Purified terephthalic acid | Adjusted for the region of production |

Table S.17: Lifecycle inventory for TA-WH.

| Terephthalic acid production – 1 kg | | |
|-------------------------------------|--|--|
| 0.000342 kg | tap water [RoW] | |
| 1.012 kg | cyclohexa-2,5-diene-1,4-dicarboxylate [US] | |
| 0.425 kg | water, completely softened [US] | |
| 0.05 kg | acetic acid, without water, in 98% solution state [RoW] | |
| 0.096 kg | oxygen, liquid [RoW] | |
| 0.0488 kg | nitrogen, liquid [RoW] | |
| 0.469 kWh | electricity, medium voltage [US] | |
| 0.637 MJ | heat, district or industrial, other than natural gas [RoW] | |
| 0.212 MJ | heat, district or industrial, other than natural gas [RoW] | |
| 0.323 MJ | heat, district or industrial, natural gas [RoW] | |
| 0.64 kg | steam, in chemical industry [RoW] | |

Table S.18: Lifecycle inventory for TA-M.

| Iso-butanol production – 1 kg | | |
|--|---|--|
| 4.013 kg | maize grain [US] | |
| 5.255 kg | tap water [RoW] | |
| 0.3 kg | sulfuric acid [RoW] | |
| 0.045 kg | sodium bicarbonate [RoW] | |
| 0.012 kg | ammonium sulfate [RoW] | |
| 0.012 kg | diammonium phosphate [RoW] | |
| 1.60 MJ | heat, district or industrial, natural gas [RoW] | |
| 0.178 kWh | electricity, medium voltage [US] | |
| Iso-butylene production – 1 kg | | |
| 1.32 kg | Isobutanol | |
| 0.5 kWh | electricity, medium voltage [US] | |
| 5.6 MJ | heat, district or industrial, natural gas [RoW] | |
| Iso-octene production – 1 kg | | |
| 2.0 kg | steam, in chemical industry [RoW] | |
| 0.0014 kg | oxygen, liquid [RoW] | |
| 0.0024 kg | tap water [RoW] | |
| 1.0 kg | Iso-butylene | |
| Iso-octane production – 1 kg | | |
| 0.982 kg | Isooctene | |
| 0.048 kWh | electricity, medium voltage [US] | |
| 0.283 MJ | heat, district or industrial, natural gas [RoW] | |
| 0.018 kg | hydrogen, liquid [RoW] | |
| Para-xylene production – 1 kg | | |
| 0.029 kWh | electricity, medium voltage [US] | |
| 2.52 MJ | heat, district or industrial, natural gas [RoW] | |
| 1.08 kg | isooctane | |
| Terephthalic acid production – 1 kg | | |
| 1 kg | Purified terephthalic acid production [RoW] | Replacing petrochemical-based para-xylene with bio-based para-xylene |

Table S.19: Lifecycle inventory for TA-WO.

| Wood feedstock handling – 907.19 kg | | |
|--|---------------------------------------|--|
| 996.86 kg | Softwood Forest Residues at Gate [US] | |
| 20.95 kg | electricity, medium voltage [US] | |
| Softwood production – 907.19 kg* | | |
| 645.34 kg | Softwood feedstock accepts [US] | |
| 13.94 kg | limestone, crushed, washed [RoW] | |
| 1360.0 kg | water, decarbonised [US] | |
| 334.92 kg | steam, in chemical industry [RoW] | |
| 13.94 kg | Sulphur [RoW] | |
| 6.98 kWh | electricity, medium voltage [US] | |
| Enzymatic hydrolysis into hydrolysate – 907.19 kg | | |
| 426.51 kg | Pulp feed [US] | |
| 0.58 kg | Enzymes [RoW] | |
| 7.45 kg | Glucose [GLO] | |
| 1.03 kg | quicklime, in pieces, loose [RoW] | |
| 0.04 kg | ammonia, anhydrous, liquid [RoW] | |
| 449.21 kg | water, decarbonised [US] | |

| | | |
|--|---|--|
| 0.97 kg | steam, in chemical industry [RoW] | |
| 0.38 kWh | electricity, medium voltage [US] | |
| Isobutanol production – 907.19 kg | | |
| 17335.28 kg | Hydrolysate [US] | |
| 34.75 kg | water, decarbonised [US] | |
| 2968.93 kg | steam, in chemical industry [RoW] | |
| 3081.17 kg | electricity, medium voltage [US] | |
| Para-xylene production – 907.19 kg | | |
| 2399.98 kg | Isobutanol | |
| 59.02 kg | water, decarbonised [US] | |
| 20.73 kg | hydrogen, gaseous [RoW] | |
| 491.02 kg | steam, in chemical industry [RoW] | |
| 812.11 kWh | electricity, medium voltage [US] | |
| Terephthalic acid production – 1 kg | | |
| 1 kg | Purified terephthalic acid production [RoW] | Replacing petrochemical-based para-xylene with bio-based para-xylene |

Table S.20: Lifecycle inventory for bio-MEG production.

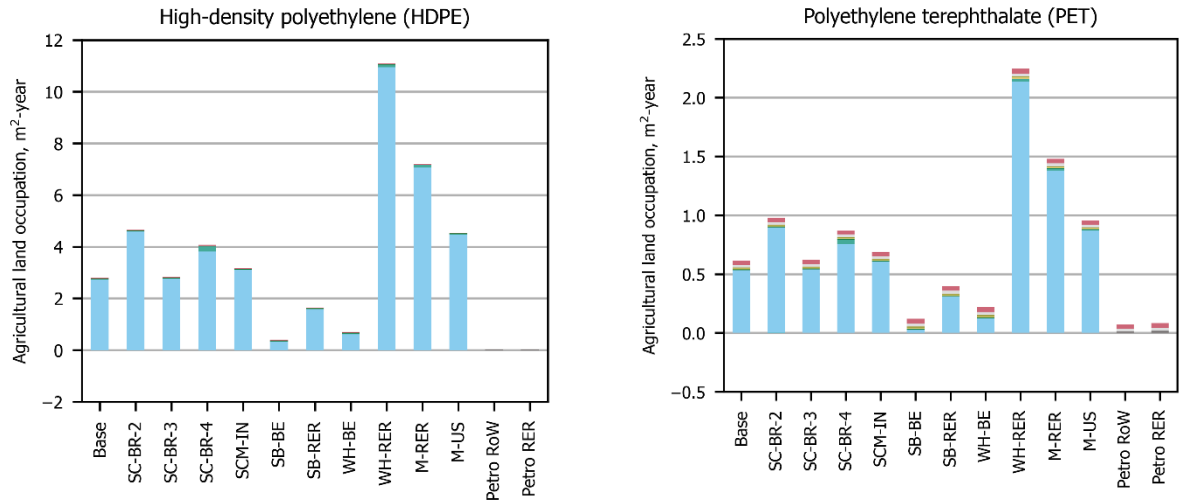
| | | |
|--|-----------------------|--|
| Ethylene oxide production – 1 kg | | |
| 1 kg | Ethylene oxide [RoW] | Replacing petrochemical ethylene with bio-based ethylene, using the local market for electricity |
| Monoethylene glycol production – 1 kg | | |
| 1 kg | Ethylene glycol [RoW] | Replacing petrochemical ethylene with bio-based ethylene, using the local market for electricity |

Table S.20: Lifecycle inventory for bio-HDPE production.

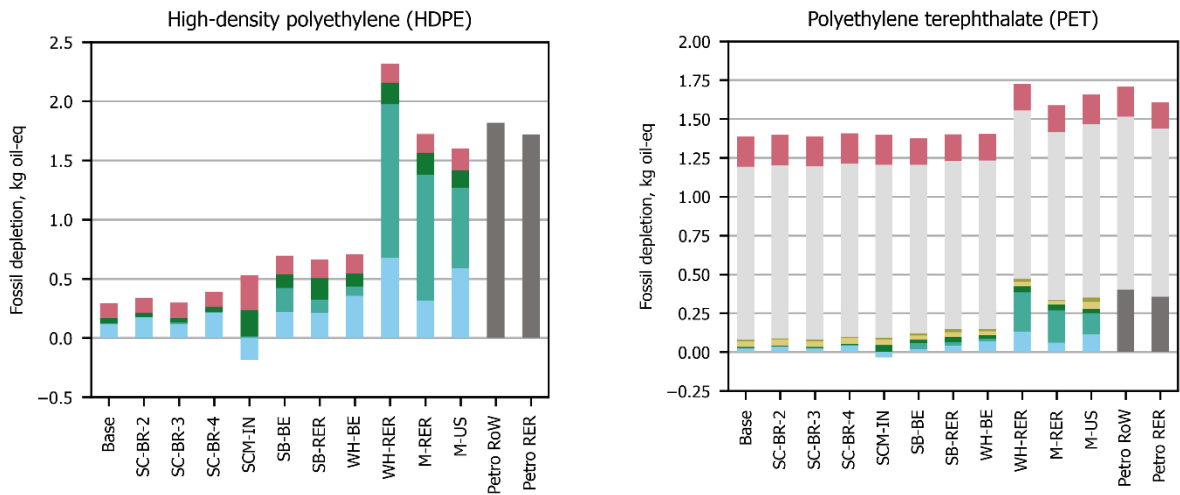
| | | |
|------------------------------|--|---|
| Polymerisation – 1 kg | | |
| Amount | Activity | Adjustments |
| 1 kg | Polyethylene, high density, granulate [RER or RoW] | Replacing petrochemical ethylene with bio-based ethylene, adjusting the location. |

Table S.21: Lifecycle inventory for bio-PET production.

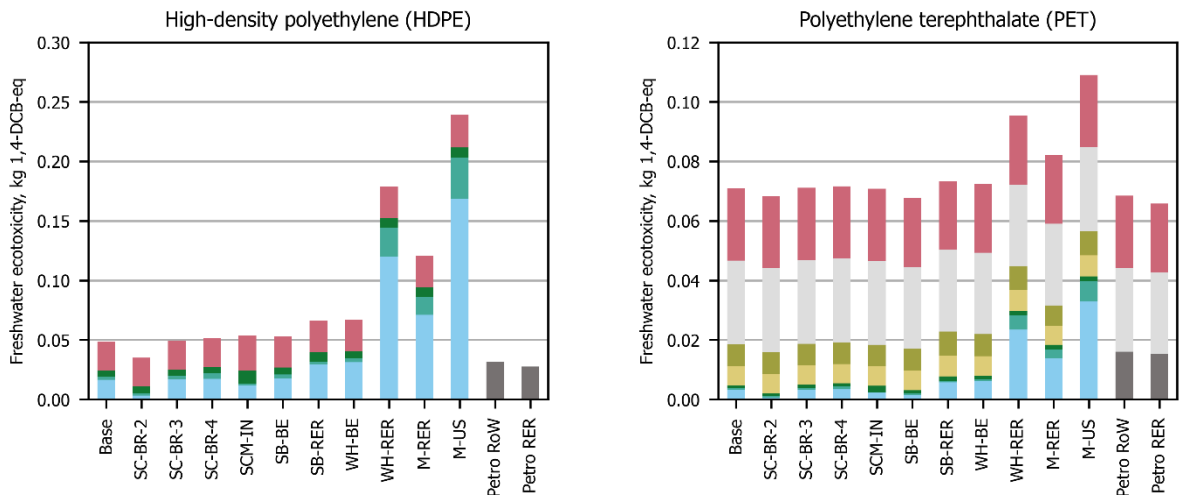
| | | |
|------------------------------|--|--|
| Polymerisation – 1 kg | | |
| Amount | Activity | Adjustments |
| 1 kg | polyethylene terephthalate, granulate, amorphous [RER] | Replacing petrochemical MEG and TA with bio-based MEG/TA and adjusting the location. |



(a) Agricultural land occupation.



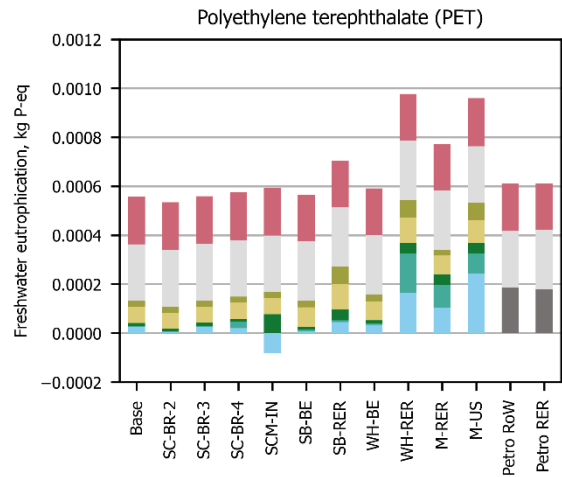
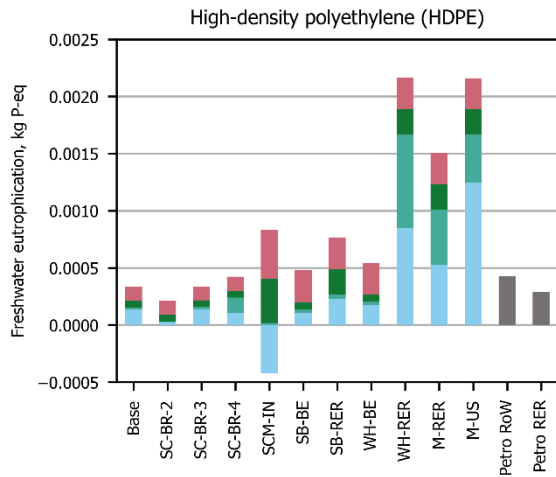
(b) Fossil depletion.



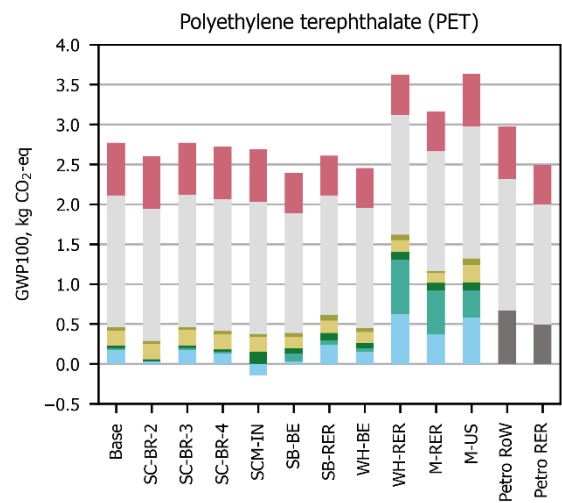
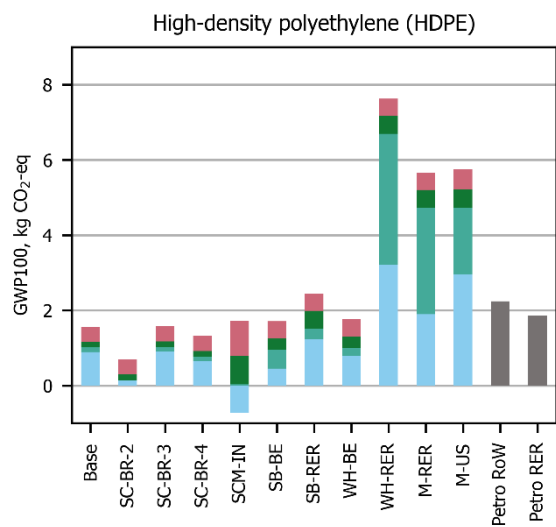
(c) Freshwater ecotoxicity.



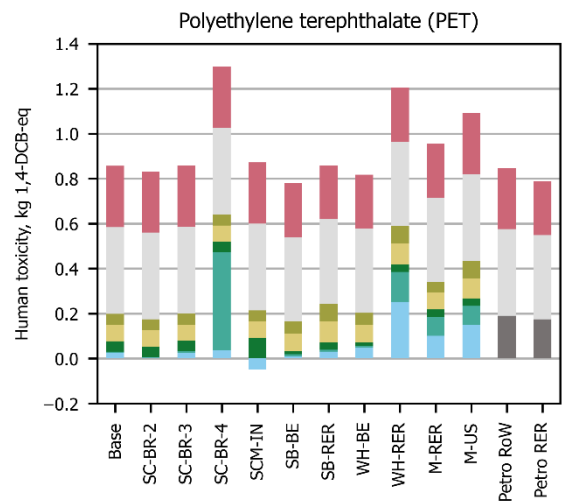
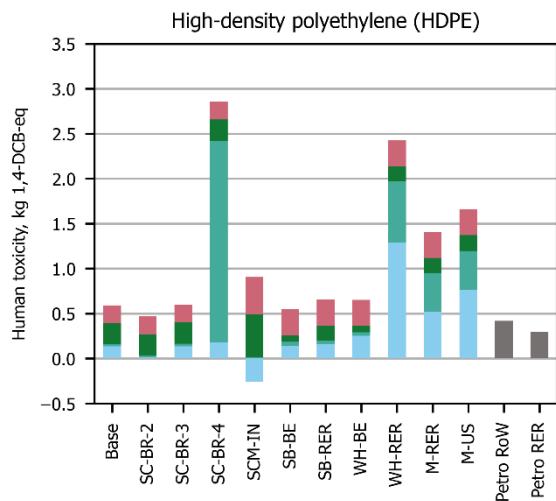
Figure S.2: Environmental impact of bio-based and petrochemical-based HDPE and PET when changing the biomass cultivation and ethanol production.



(d) Freshwater eutrophication.



(e) Global warming potential (GWP100).



(f) Human toxicity.

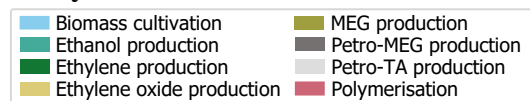
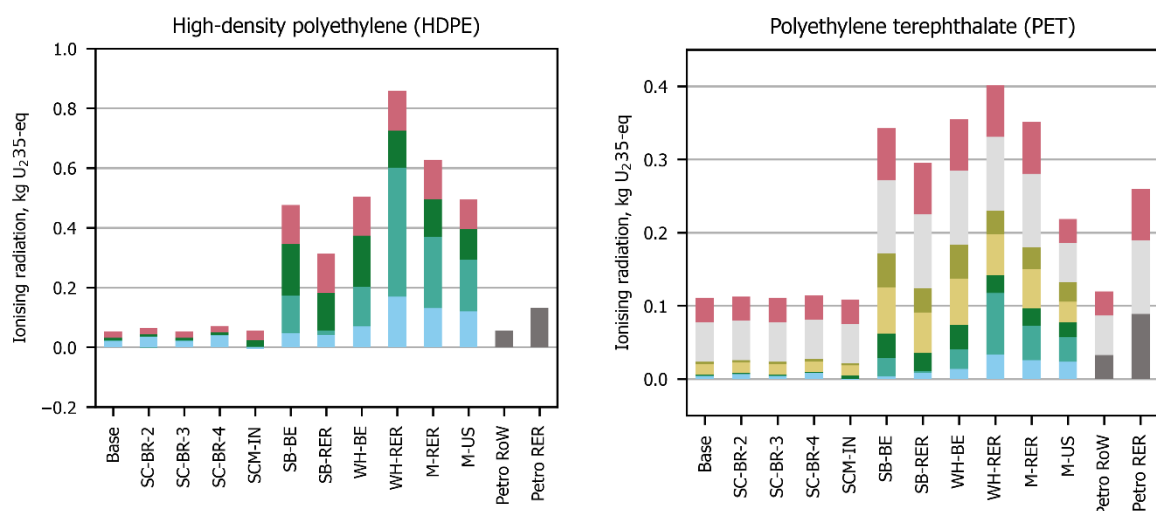
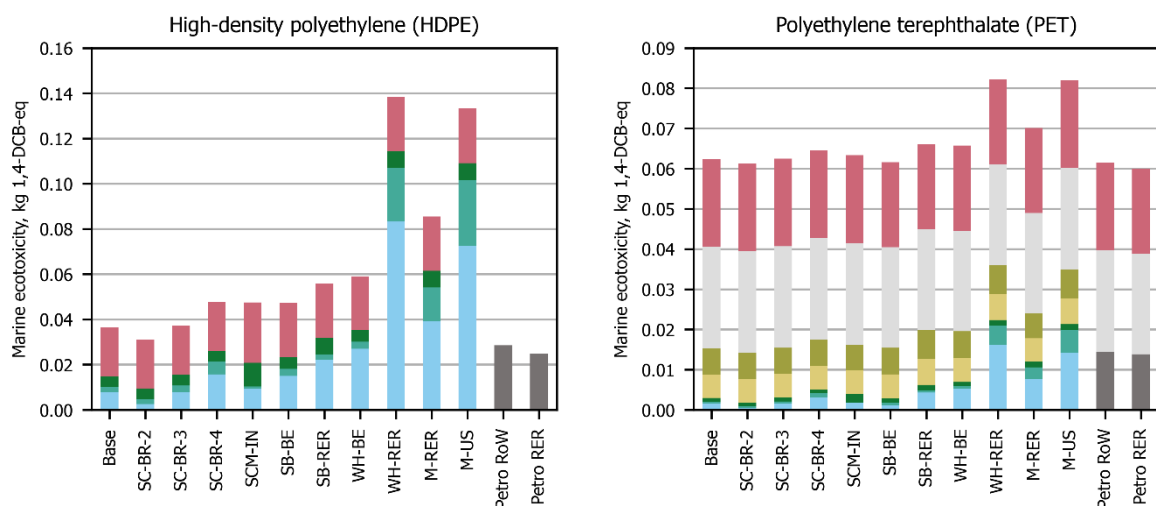


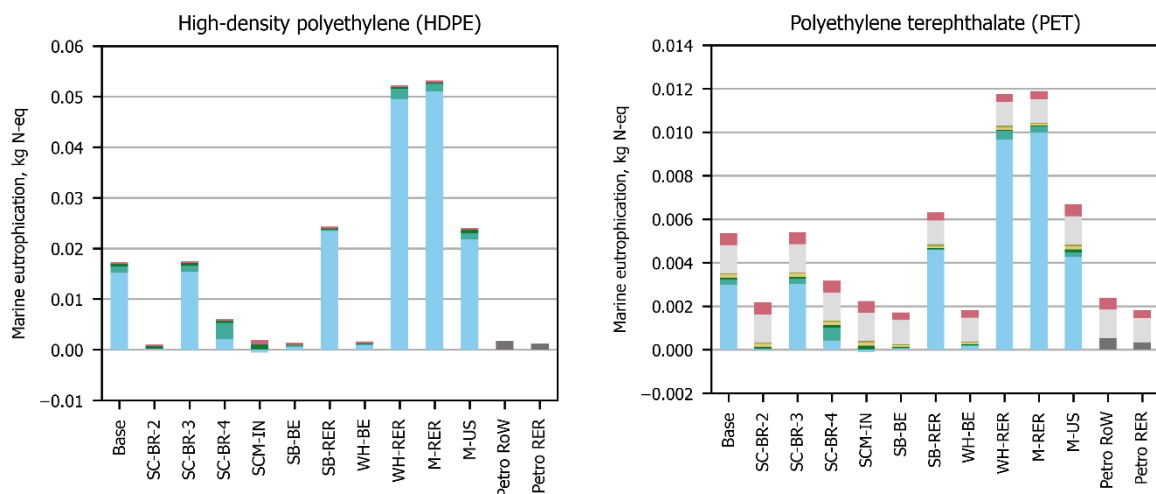
Figure S.2 continued.



(g) Ionising radiation.



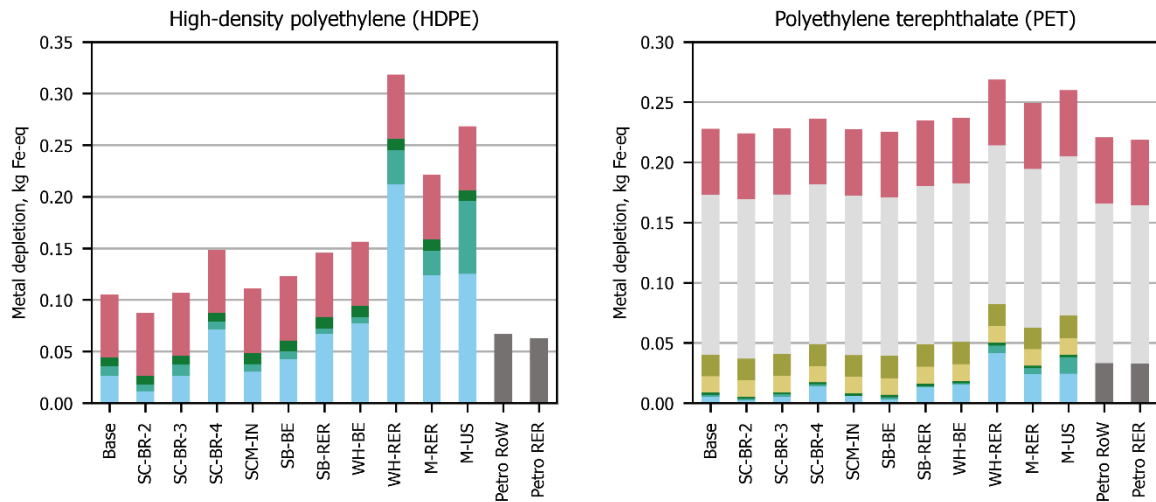
(h) Marine ecotoxicity.



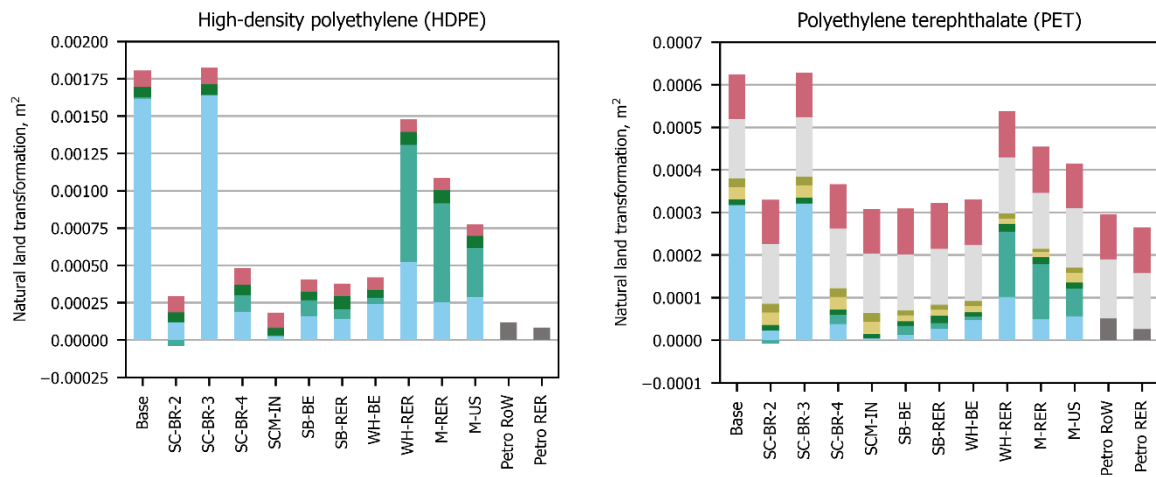
(i) Marine eutrophication.



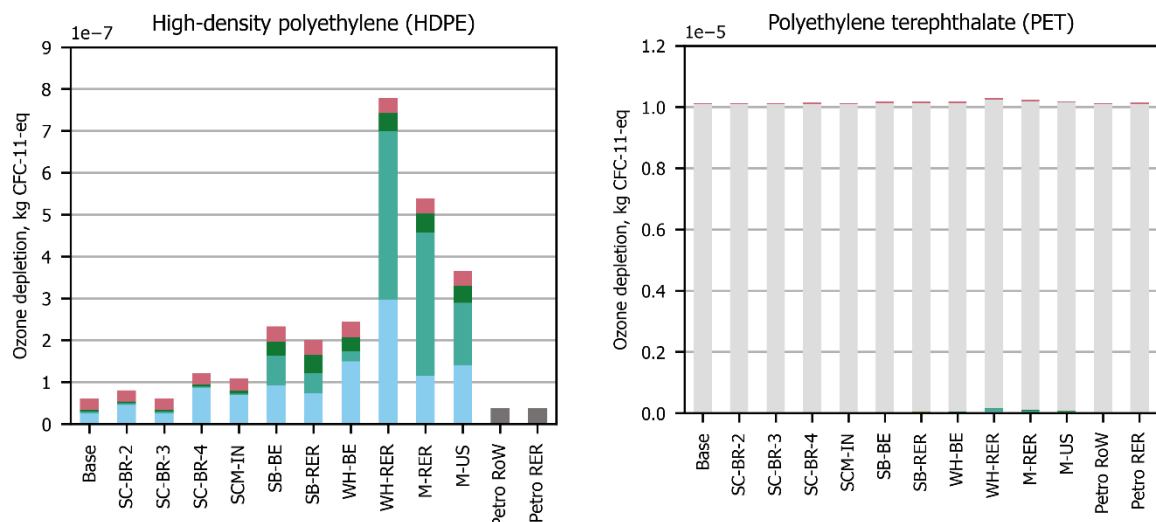
Figure S.2 continued.



(j) Metal depletion.



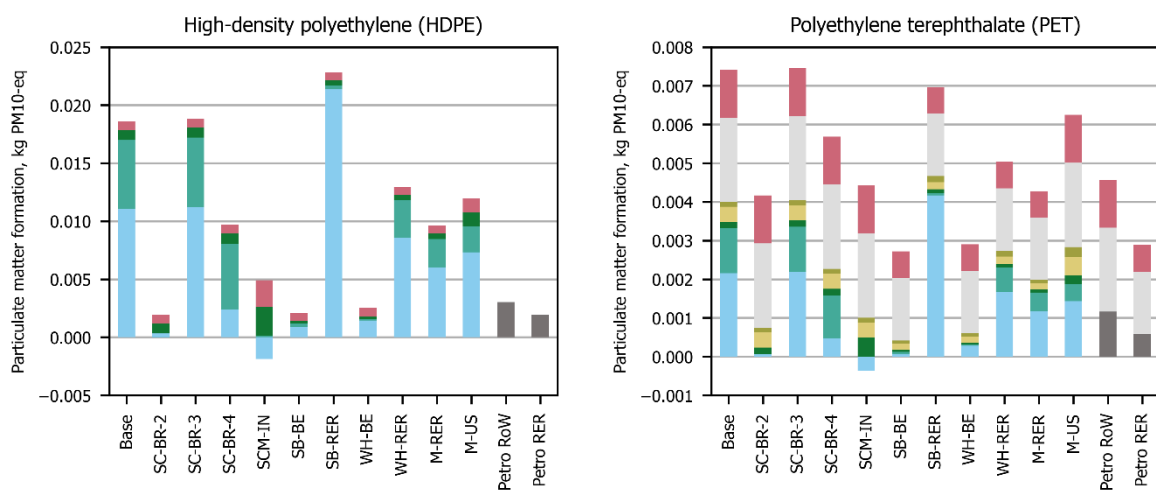
(k) Natural land transformation.



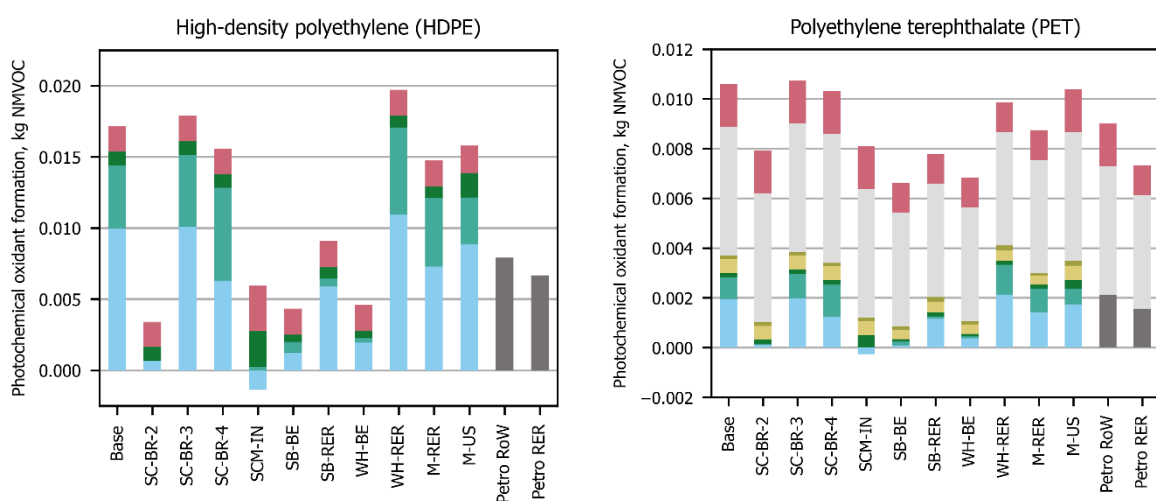
(l) Ozone depletion.



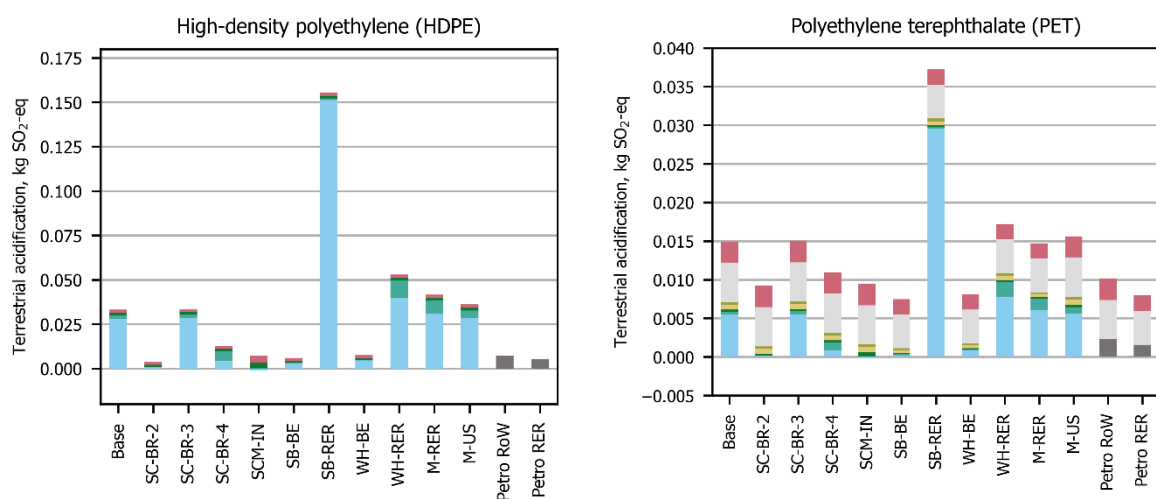
Figure S.2 continued.



(m) Particulate matter formation.



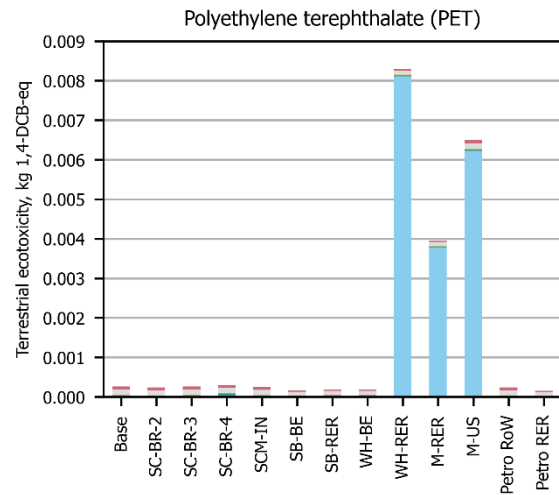
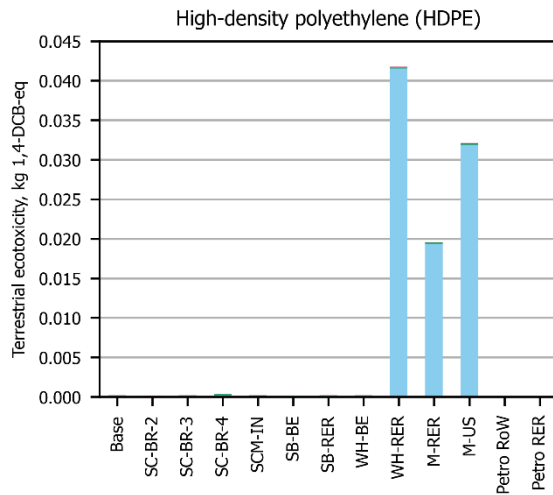
(n) Photochemical oxidant formation.



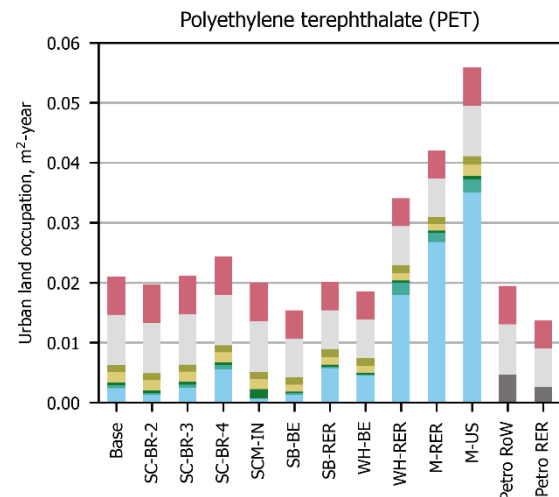
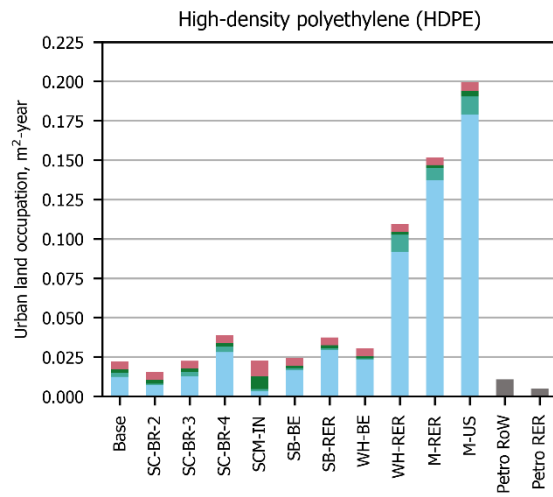
(o) Terrestrial acidification.



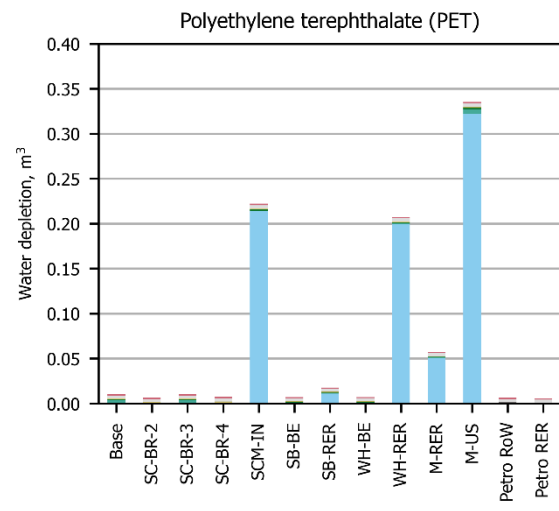
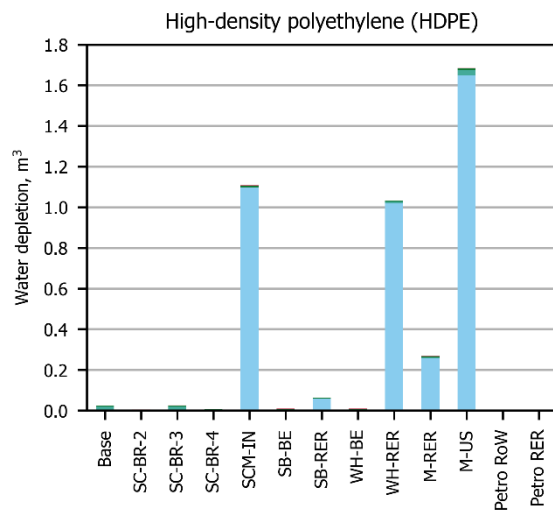
Figure S.2 continued.



(p) Terrestrial ecotoxicity.



(q) Urban land occupation.



(r) Water depletion.

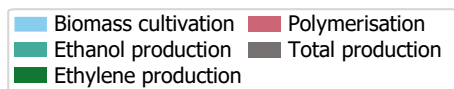
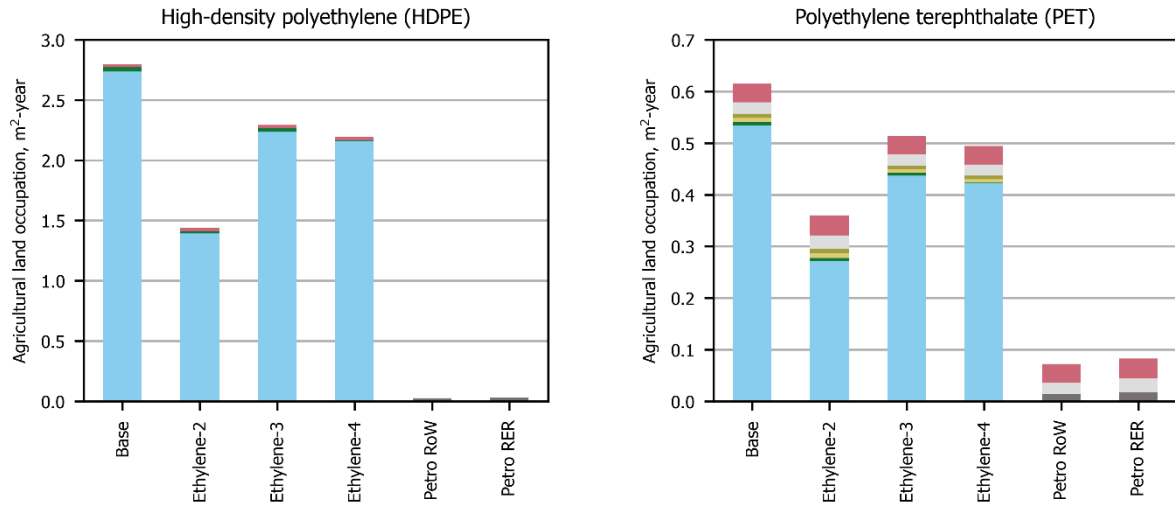
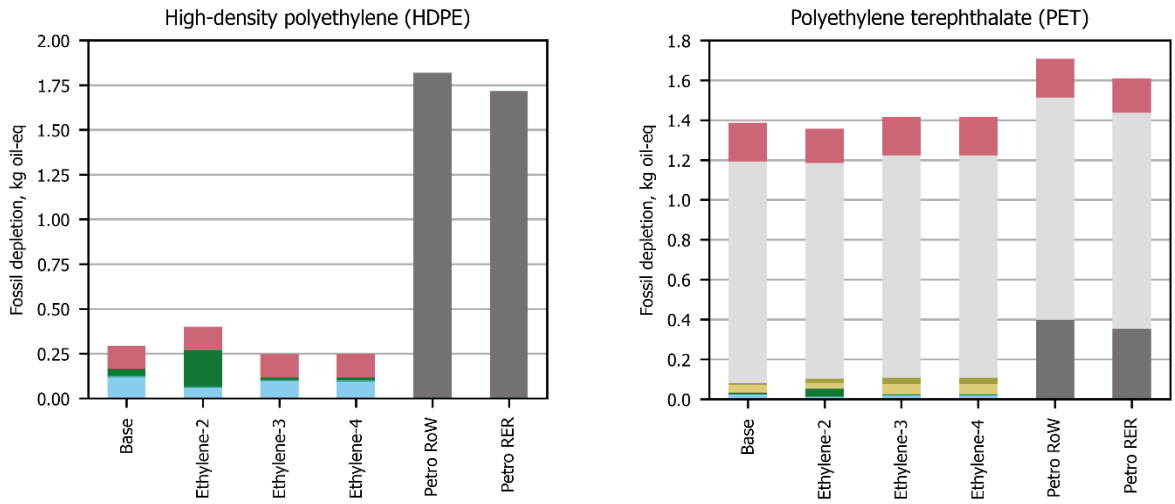


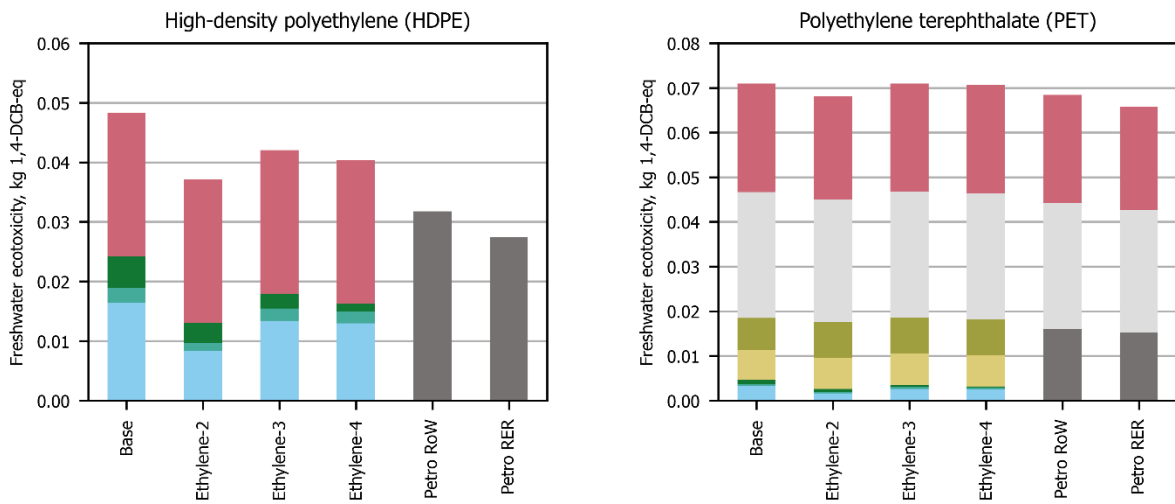
Figure S.2 continued.



(a) Agricultural land occupation.



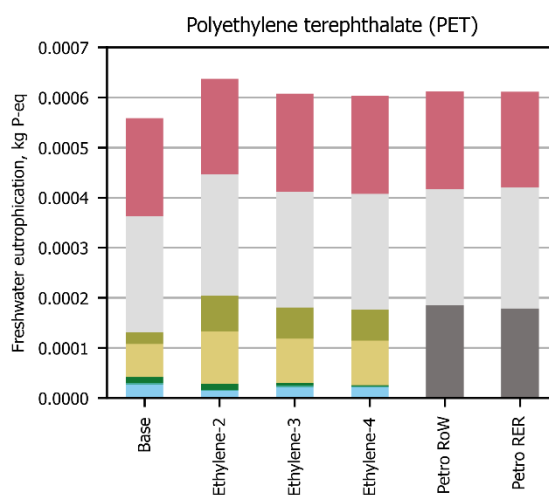
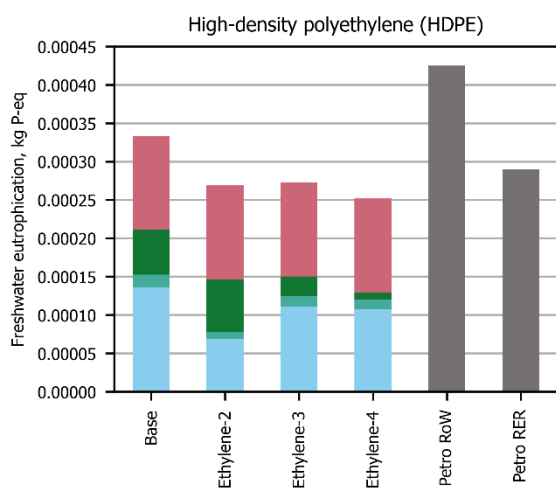
(b) Fossil depletion.



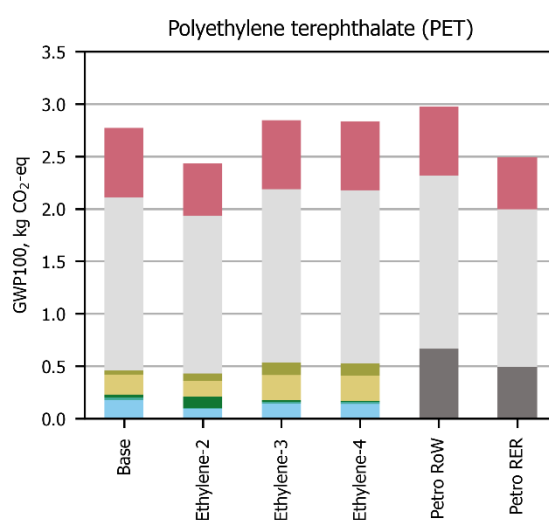
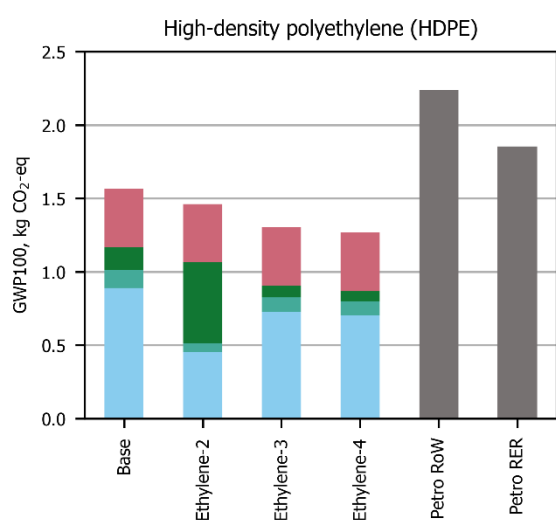
(c) Freshwater ecotoxicity.



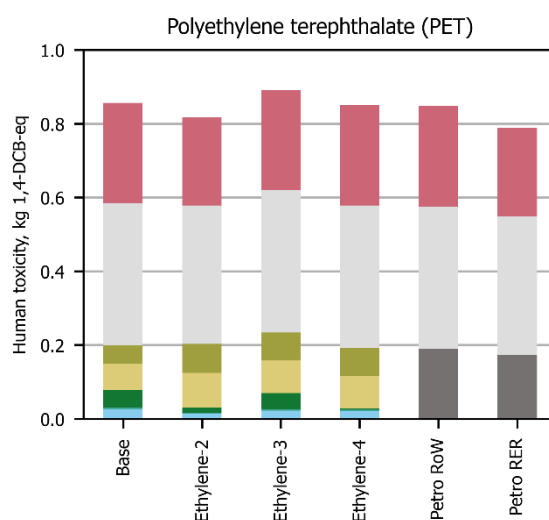
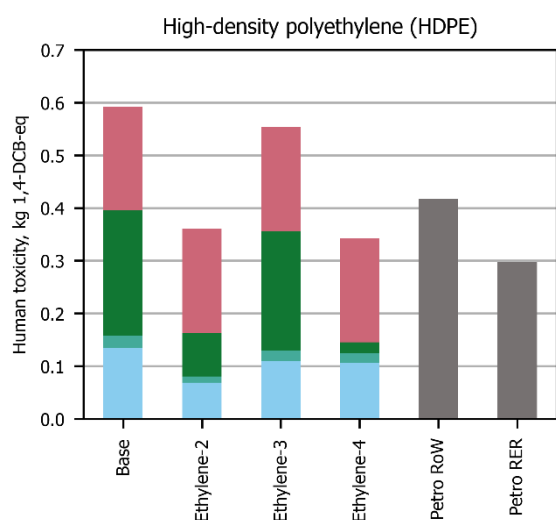
Figure S.3: Environmental impact of bio-based and petrochemical-based HDPE and PET when changing the ethylene production.



(d) Freshwater eutrophication.



(e) Global warming potential (GWP100).



(f) Human toxicity.

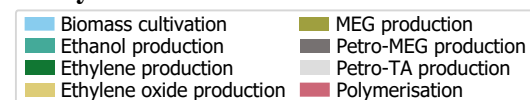
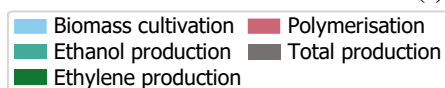
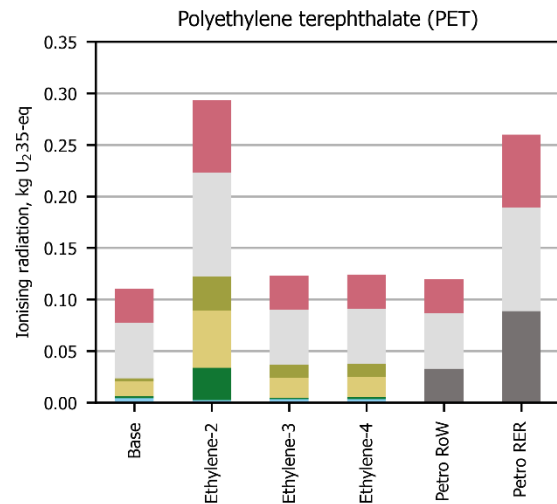
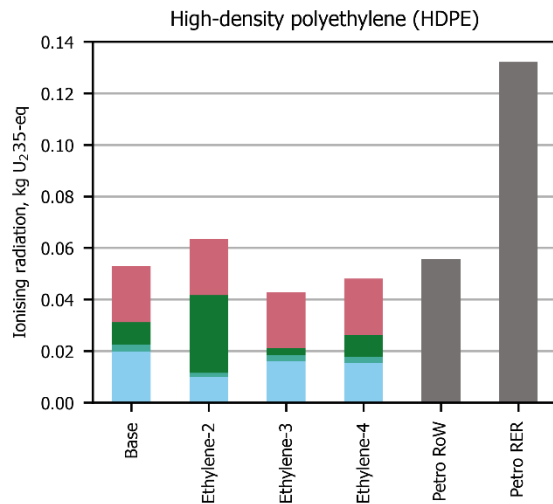
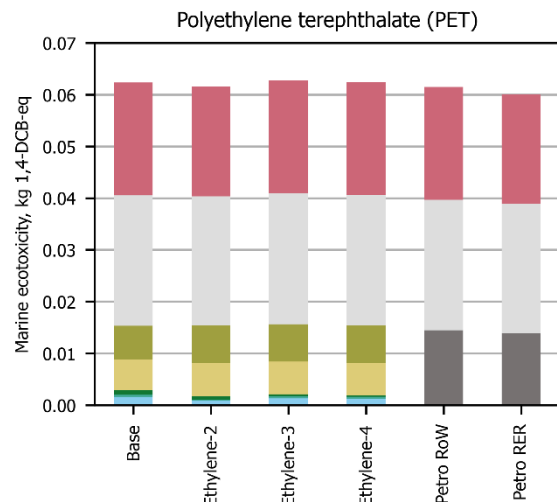
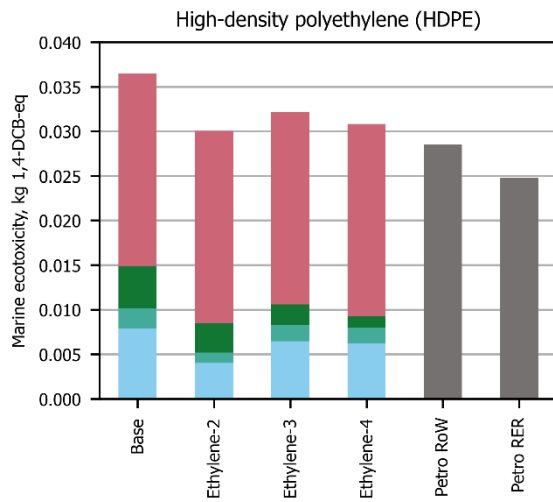


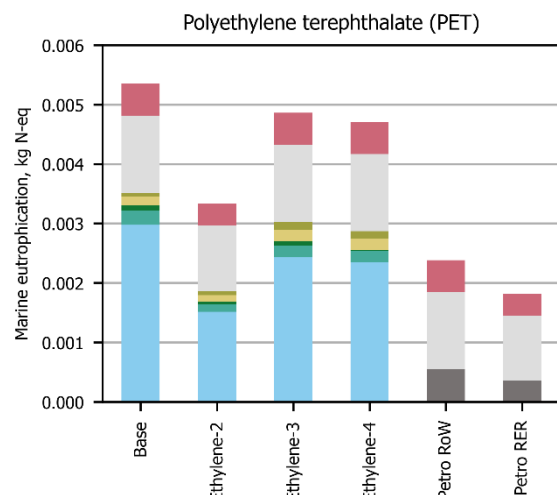
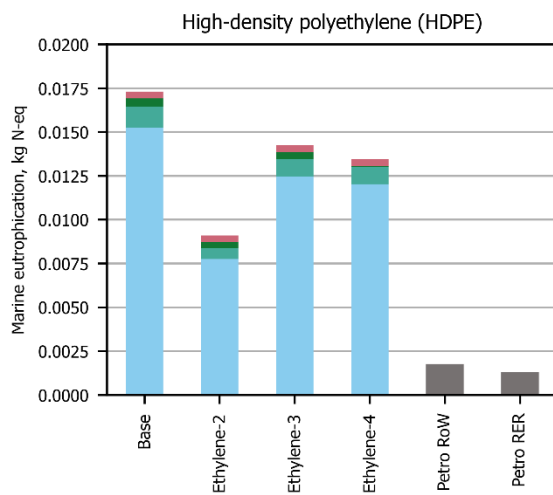
Figure S.3 continued.



(g) Ionising radiation.



(h) Marine ecotoxicity.



(i) Marine eutrophication.

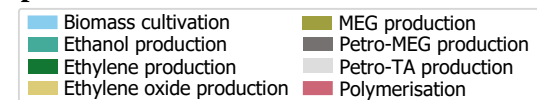
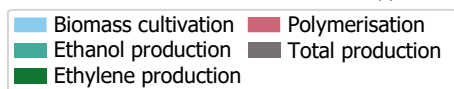
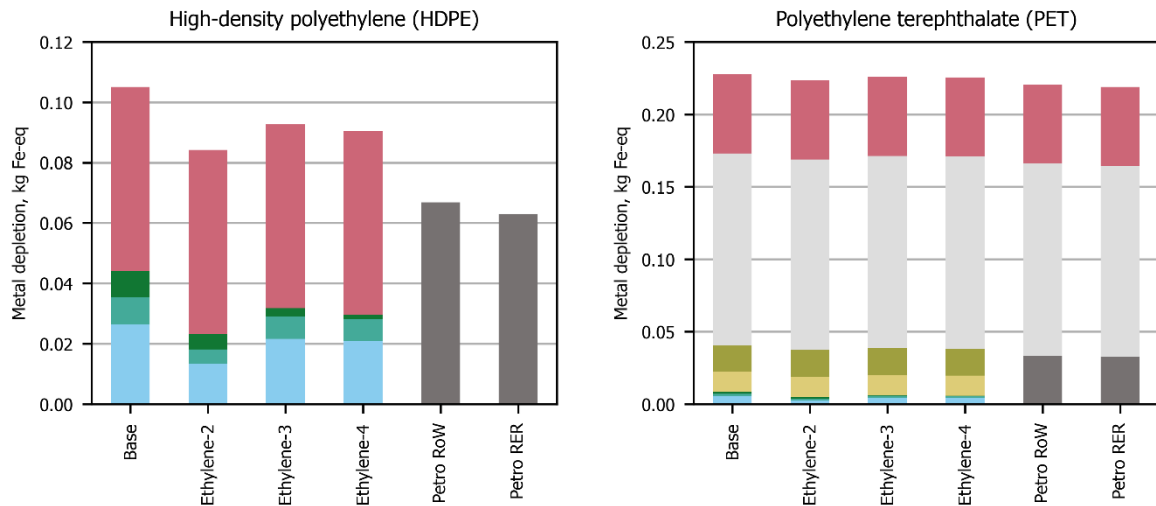
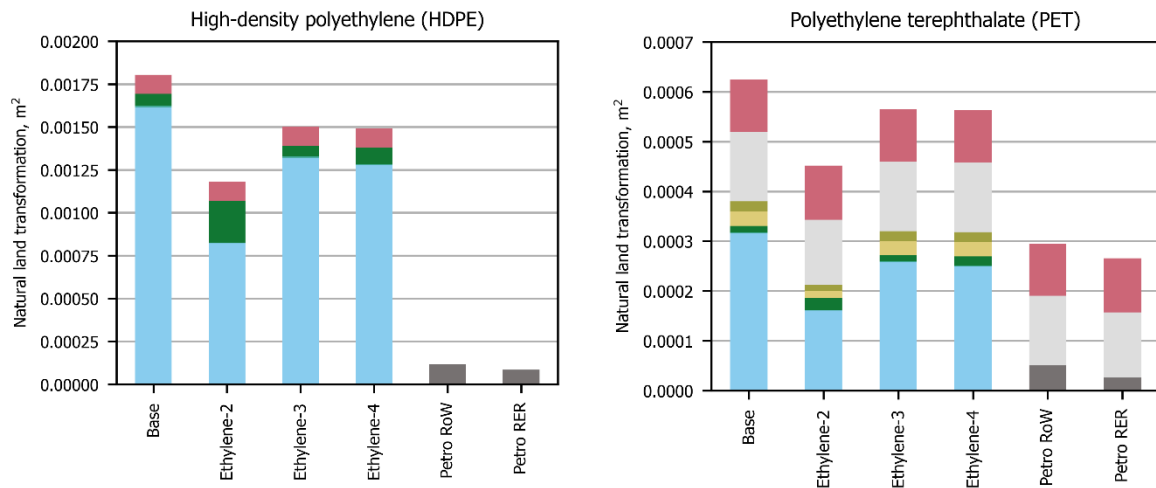


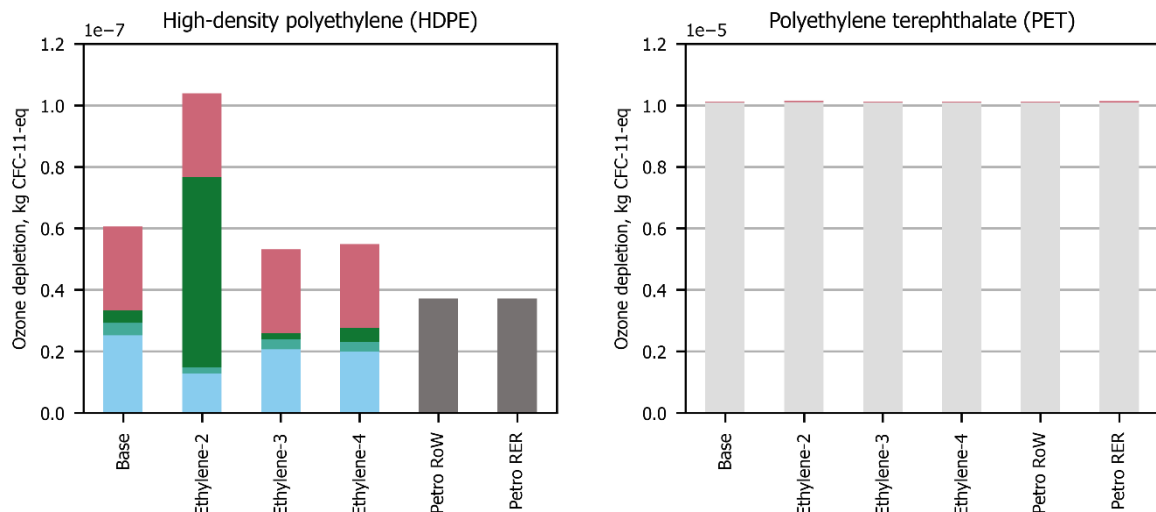
Figure S.3 continued.



(j) Metal depletion.



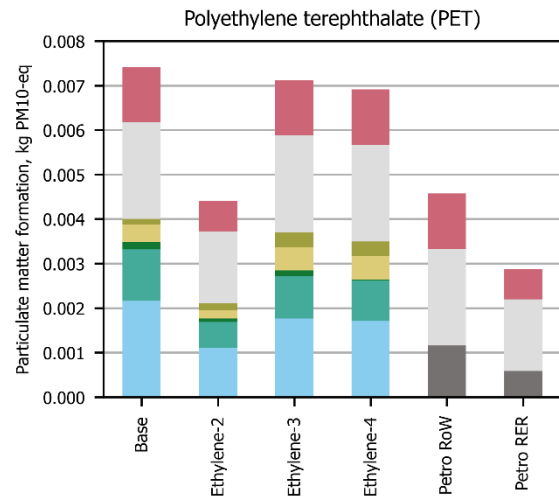
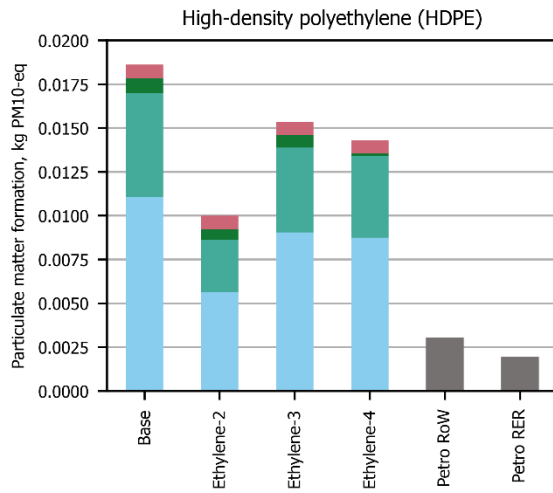
(k) Natural land transformation.



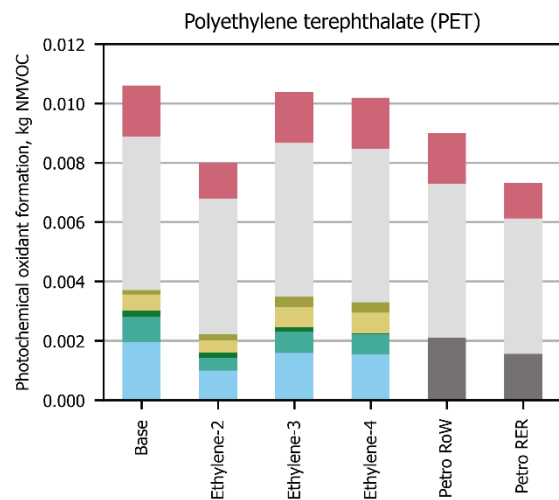
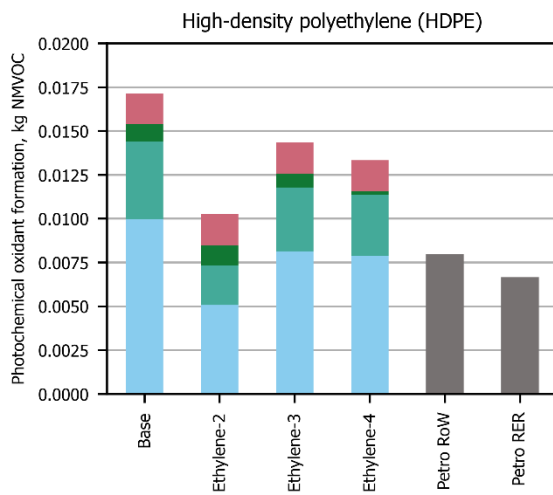
(l) Ozone depletion.



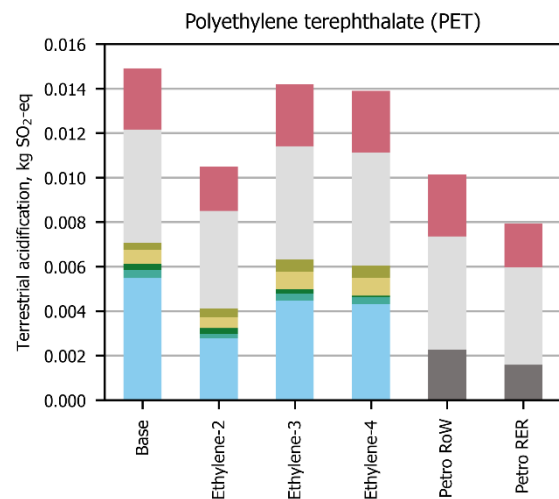
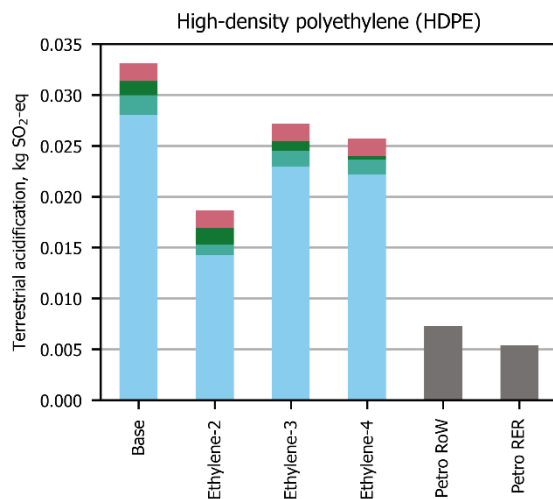
Figure S.3 continued.



(m) Particulate matter formation.



(n) Photochemical oxidant formation.



(o) Terrestrial acidification.

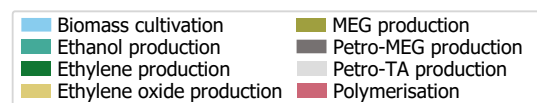
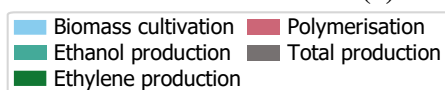
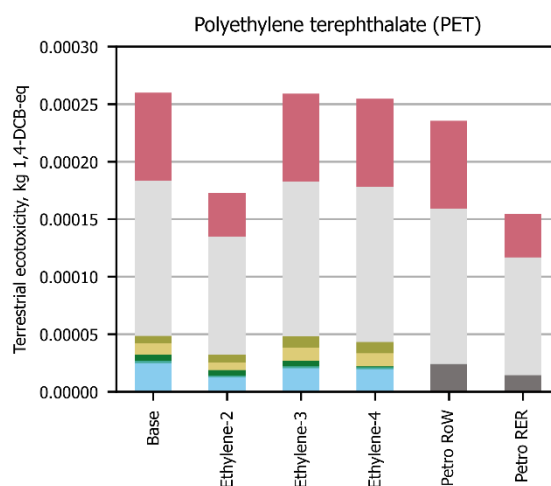
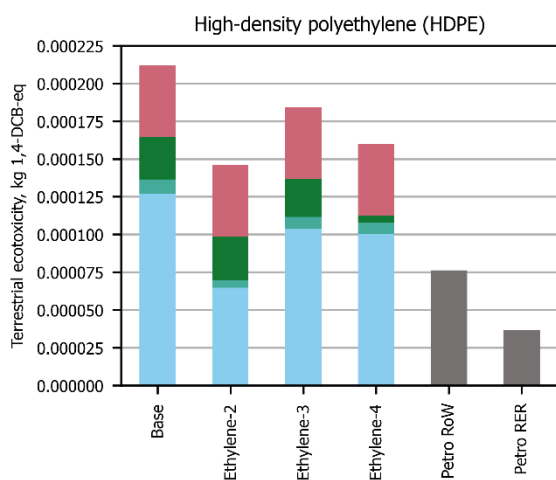
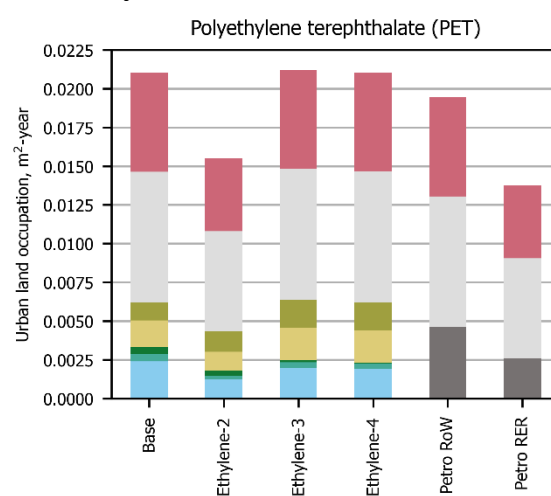
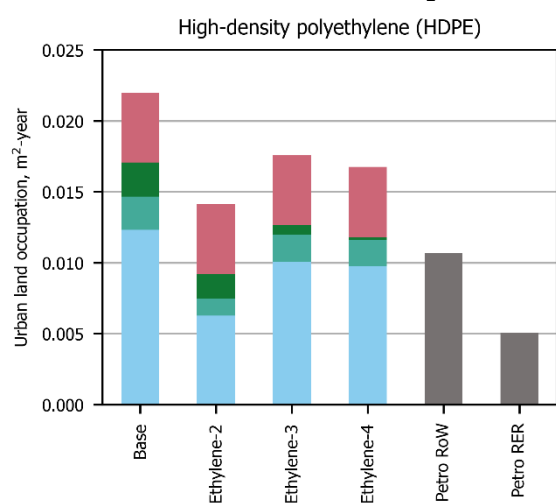


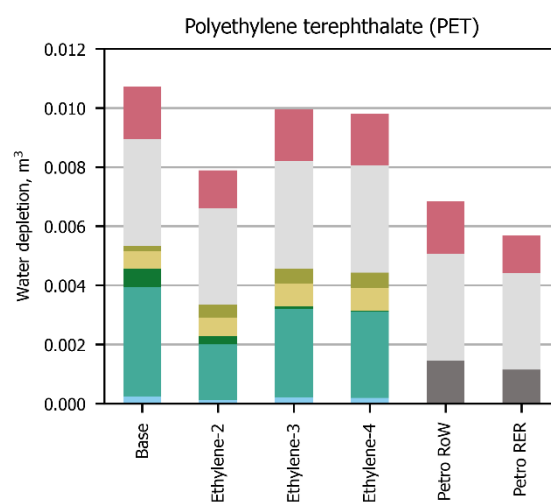
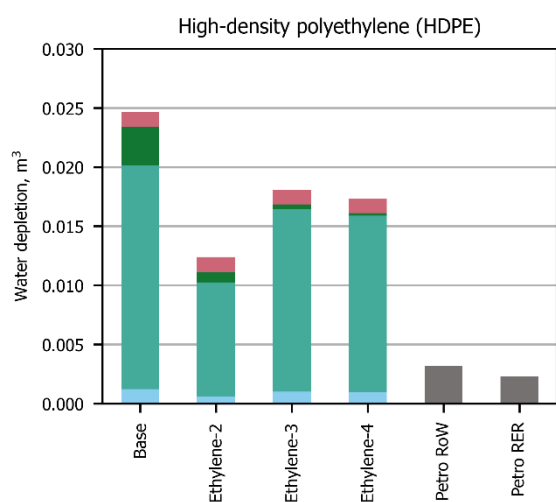
Figure S.3 continued.



(p) Terrestrial ecotoxicity.



(q) Urban land occupation.



(r) Water depletion.

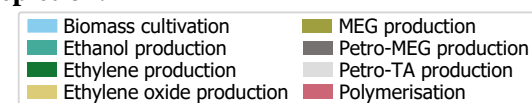


Figure S.3 continued.

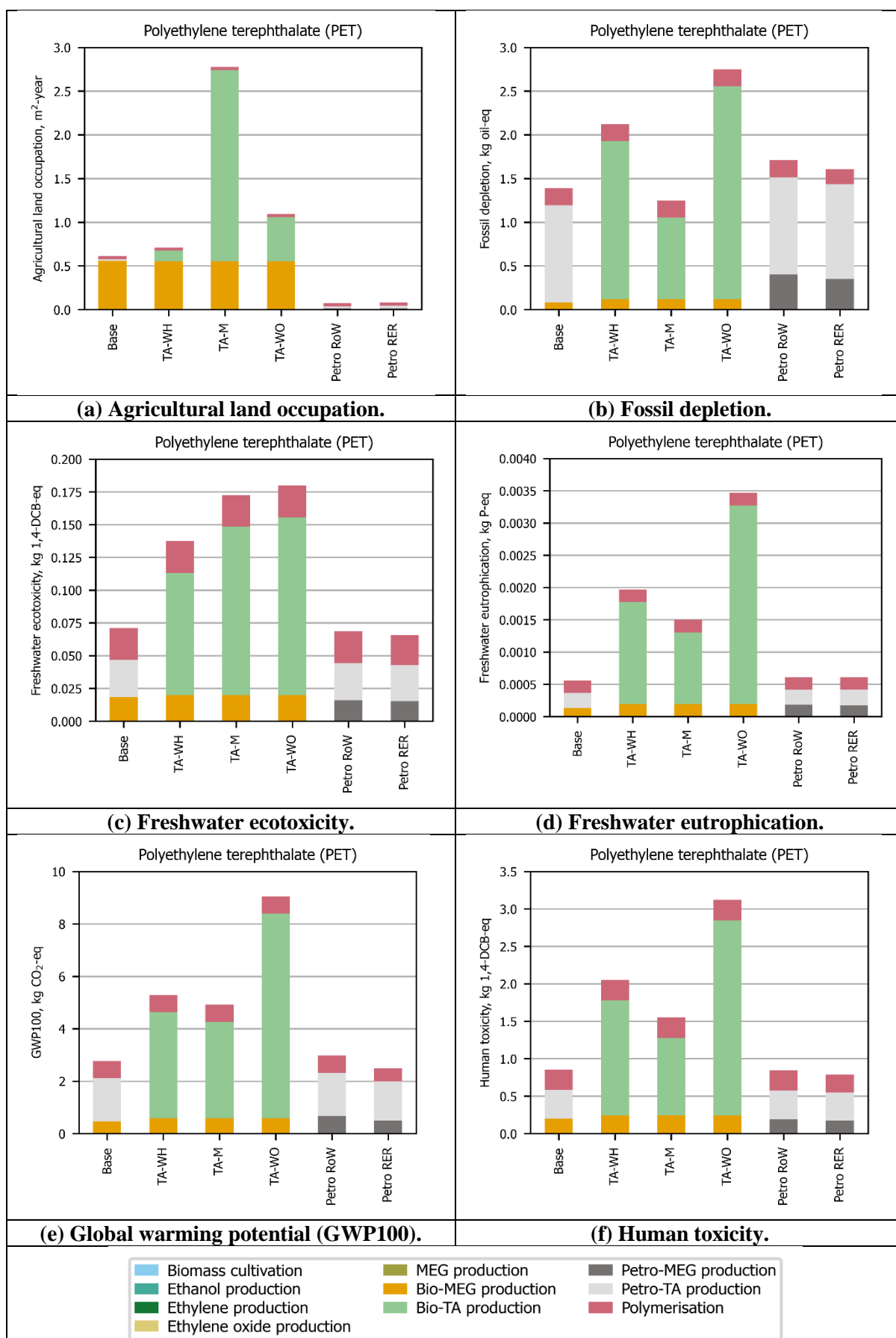


Figure S.4: Environmental impact of bio-based and petrochemical-based PET when changing TA production.

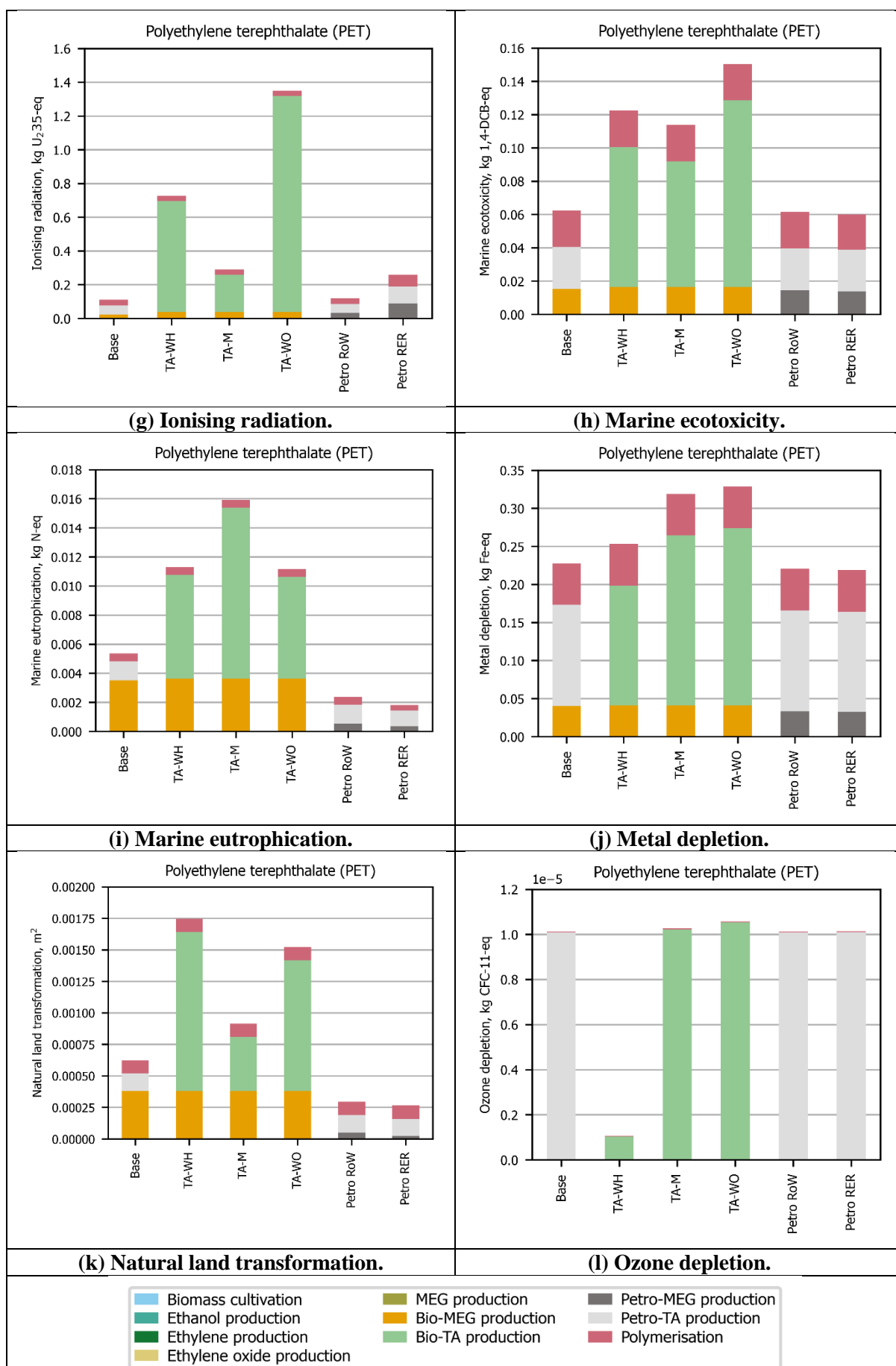


Figure S.4 continued.

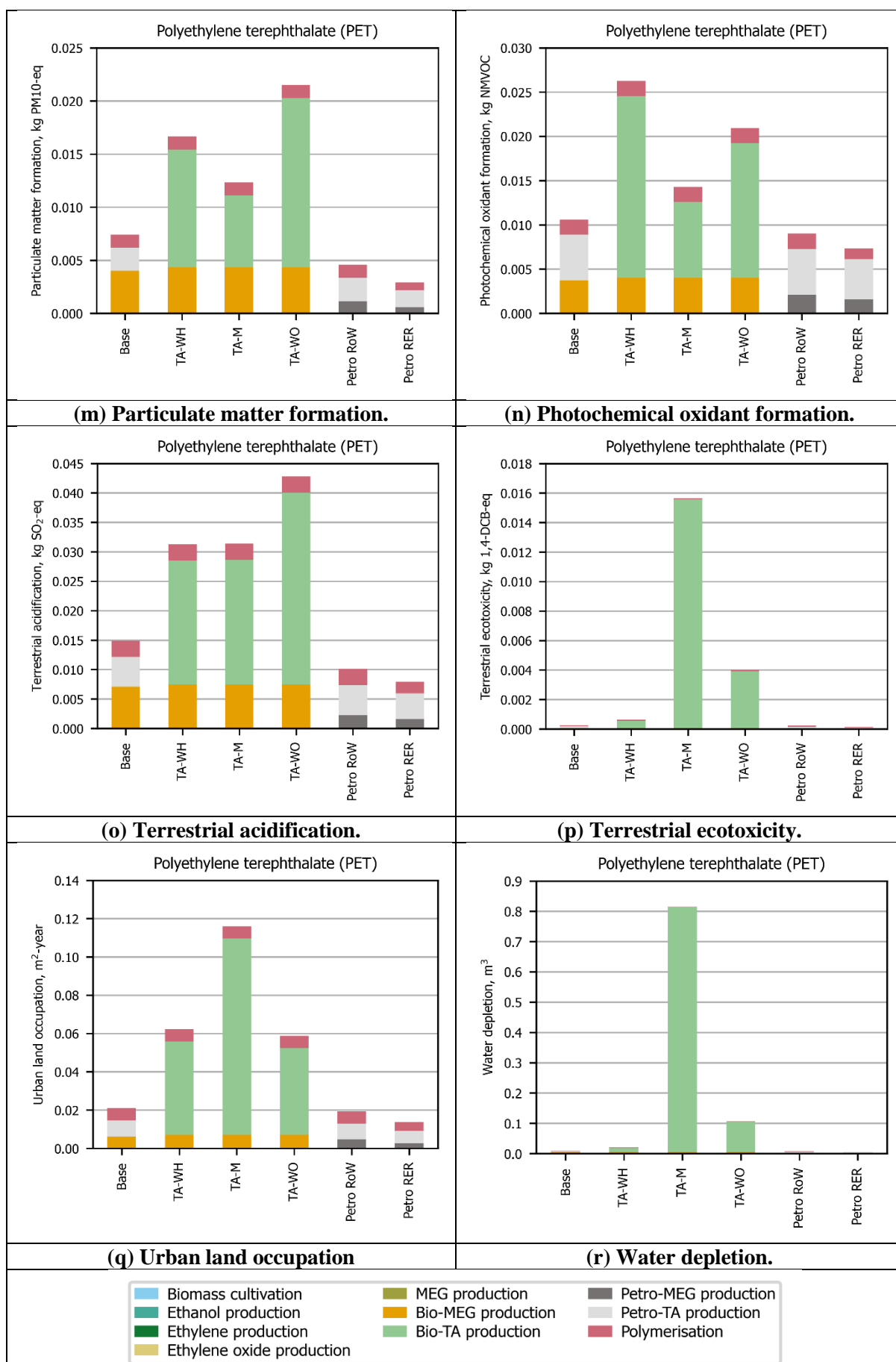


Figure S.4 continued.